LISTING OF CLAIMS

1. (currently amended) A process for selectively activating a dewaxing catalyst for the catalytic dewaxing of a waxy hydrocarbon feed which comprises: contacting the dewaxing catalyst which is a molecular sieve in the hydrogen form on an alumina or alumina-containing binder with a carrier feed containing about 100 wppm to 10,000 wppm measured as oxygen of at least one oxygenate at a temperature of from 120 to 400°C, a hydrogen pressure of from 101 to 20786 kPa, provided that the mode of dewaxing is by isomerizing waxy molecules and the selectivity of the dewaxing catalyst is improved by isomerizing at least 4 relative % more of the wax component of the waxy molecules in the hydrocarbon feed into lube isomerate.

2. (original) The process of claim 1 wherein the dewaxing catalyst contains at least one molecular sieve containing at least one 10 or 12 ring channel.

3. (original) The process of claim 2 wherein the molecular sieve is at least one of ZSM-5, ZSM-11, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57, ferrierite, EU-1, NU-87, ECR-42, SAPO-11, SAPO-41, ITQ-13 or MCM-71.

4. (original) The process of claim 2 wherein the molecular sieve is at least one of zeolite beta, ZSM-12, MCM-68, SAPO-5, SAPO-31, MAPO-36, ZSM-18, offretite, mordenite or faujasite.

5. (original) The process of claim 3 wherein the molecular sieve is ZSM-48.

6. (original) The process of claim 1 wherein the oxygenate is at least one alcohol, carboxylic acid, ester, aldehyde, ketone or ether.

7. (original) The process of claim 1 wherein the oxygenate is water.

8. (cancelled)

9. (original) The process of claim 1 wherein the carrier feed is the wax containing hydrocarbon feed.

10. (original) The process of claim 1 wherein the dewaxing catalyst is sulfided, reduced, or sulfided and reduced.

11. (original) The process of claim 1 wherein the dewaxing catalyst bears a metal hydrogenation component.

12. (original) The process of claim 11 wherein the metal hydrogenation component is at least one Group 9 or 10 noble metal.

13. (currently amended) A process for selectively activating a dewaxing catalyst for the catalytic dewaxing of a wax containing hydrocarbon feed which comprises: contacting the dewaxing catalyst which contains at least one molecular sieve in the hydrogen form on an alumina or alumina-containing binder and containing at least one 10 or 12 channel with a carrier feed containing at least about 100 wppm to 10,000 wppm of oxygenate, measured as oxygen, at a temperature of from 120 to 400°C and a hydrogen pressure of from 101 to 20786 kPa, provided that the mode of dewaxing is by isomerizing waxy molecules and

the selectivity of the dewaxing catalyst is improved by isomerizing at least 4 relative % more of the wax into lube isomerate.

14. (original) The process of claim 13 wherein the molecular sieve is at least one of ZSM-5, ZSM-11, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57, ferrierite, EU-1, NU-87, SAPO-11, SAPO-41, ITQ-13 or MCM-71.

15. (original) The process of claim 13 wherein the molecular sieve is at least one of zeolite beta, ZSM-12, MCM-68 SAPO-5, SAPO-31, MAPO-36, ZSM-18, offretite, mordenite or faujasite.

16. (original) The process of claim 14 wherein the molecular sieve is ZSM-48.

17. (original) The process of claim 13 wherein the oxygenate is at least one alcohol, carboxylic acid, ester, aldehyde, ketone or ether.

18. (original) The process of claim 13 wherein the oxygenate is water.

19. (original) The process of claim 13 wherein the carrier feed is the wax containing hydrocarbon feed.

20. (original) The process of claim 13 wherein the dewaxing catalyst is sulfided, reduced, or sulfided and reduced.

21. (currently amended) A process for selectively activating a dewaxing catalyst for catalytic dewaxing of a wax containing hydrocarbon feed which

comprises: contacting the dewaxing catalyst which contains at least one molecular sieve in the hydrogen form on an alumina or alumina-containing binder and containing at least one 10 or 12 channel with a carrier feed containing at least about 100 wppm to 10,000 wppm, measured as oxygen, of an oxygenate which is at least one alcohol, carboxylic acid, ester, aldehyde, ketone or ether at a temperature of from 120 to 400°C and a hydrogen pressure of from 101 to 20786 kPa, provided that the mode of dewaxing is by isomerizing waxy molecules and the selectivity of the dewaxing catalyst is improved by isomerizing at least 4 relative % more of the wax into lube isomerate.

22. (original) The process of claim 21 wherein the molecular sieve is at least one of ZSM-5, ZSM-11, ZSM-22, ZSM-23, ZSM-35, ZSM-48, ZSM-57, ferrierite, EU-1, NU-87, SAPO-11, SAPO-41, ITQ-13 or MCM-71.

23. (original) The process of claim 21 wherein the molecular sieve is at least one of zeolite beta, ZSM-12, MCM-68 SAPO-5, SAPO-31, MAPO-36, ZSM-18, offretite, mordenite or faujasite.

24. (original) The process of claim 22 wherein the molecular sieve is ZSM-48.

25. (original) The process of claim 19 wherein the carrier feed is the wax containing hydrocarbon feed.

26. (original) The process of claim 21 wherein the dewaxing catalyst is sulfided, reduced, or sulfided and reduced.

27. (original) The process of claim 21 wherein the dewaxing catalyst bears a metal hydrogenation component.

28. (original) The process of claim 27 wherein the metal hydrogenation component is at least one Group 9 or 10 noble metal.

29. (currently amended) A process for selectively activating a ZSM-48 catalyst for the catalytic dewaxing of a wax containing hydrocarbon feed which comprises: contacting ZSM-48 in the hydrogen form on an alumina or alumina-containing binder with a carrier feed containing at least about 100 wppm to 10,000 wppm, measured as oxygen, of an oxygenate which is at least one alcohol, carboxylic acid, ester, aldehye, ketone or ether at a temperature of from 120 to 400 °C and a hydrogen pressure of from 101 to 20786 kPa, provided that the mode of dewaxing is by isomerizing waxy molecules and the selectivity of the ZSM-48 catalyst is improved by isomerizing at least 4 relative % more of the wax into lube isomerate.

30. (original) The process of claim 29 wherein the carrier feed is the wax containing hydrocarbon feed.

31. (original) The process of claim 29 wherein the ZSM-48 catalyst is sulfided, reduced, or sulfided and reduced.

32. (original) The process of claim 29 wherein the ZSM-48 catalyst bears a metal hydrogenation component.

33. (original) The process of claim 32 wherein the metal hydrogenation component is at least one Group 9 or 10 noble metal.

34. (currently amended) A process for selectively activating a dewaxing catalyst for the catalytic dewaxing of a wax containing hydrocarbon feed which comprises: contacting the dewaxing catalyst which contains at least one molecular sieve in the hydrogen form on an alumina or alumina-containing binder and containing at least one 10 or 12 channel with a carrier feed containing at least about 100 wppm to 10,000 wppm, measured as oxygen of an oxygenate which is water at a temperature of from 120 to 400°C and a hydrogen pressure of from 101 to 20786 kPa, provided that the mode of dewaxing is by isomerizing waxy molecules and the selectivity of the dewaxing catalyst is improved by isomerizing at least 4 relative % more of wax component into lube isomerate.

35. (cancelled)